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Dye-sensitized TiO₂ film with bifunctionalized zones for photocatalytic degradation of 4-cholophenol

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ABSTRACT

A new strategy to photocatalytic degradation of 4-cholophenol (4-CP) under visible light irradiation was described. The TiO_2 film deposited on an ordinary glass sheet was distributed into two zones. One zone was sensitized by N719 dye and fabricated to be a sandwich type cell with a similar structure of dye-sensitized solar cells. The other zone was inserted into pollutants solution for degradation. A highly oxidized overvoltage anode was achieved from the dye-sensitized zone. The bifunctionalized TiO_2 film and the anode could degrade 4-chlorophenol in two separate reactors with 97% and 96% removal of 4-CP after 5 h, respectively. The degradation efficiency could be improved by addition of FeSO₄. The as-prepared bifunctionalized TiO_2 film was comparably stable in the process of degradation.

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1. Introduction

With rapid industrialization in the world, chemical pollutants, such as dyes, sulphates and toxic compounds, are dumped into rivers and are polluting soil and water. These pollutants affecting on environment is particularly serious in developing countries. Moreover, there is a continually growing problem due to the rising population and increasing demands for water sources. Efforts should be made on the development of various treatment technologies to decrease environmental pollution. Heterogeneous photocatalysis using titanium dioxide has attracted extensive attention in the field of degradation of chemical pollutants in aqueous phases [1-3]. Though titanium dioxide possesses merits of low-cost, non-toxicity, inert nature and long-term stability, two major problems of the recombination of photogenerated charge carriers and the filtration step of suspended particles after water treatment obstruct the practical application in the environmental areas [4-7]. Photoelectrocatalytic (PEC) process has proven to be an efficient method to solve these two problems, which is through immobilization of TiO₂ on a conducting substrate and application of a potential bias [8,9]. However, the wide band gap of TiO₂ can only capture about 5% of solar irradiance on earth's surface. To obtain a more efficient utilization of solar irradiation, many attempts,

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such as metal or nonmetal elements doping [10–15], were made to shift its photocatalytic activity from UV illumination to the visible region. Although exciting improvements on the photocatalytic activity of TiO_2 under visible light irradiation, have been achieved through those modifications, some problems for doped materials with thermal instability and carrier-recombination probability still exist and affect practical utilization.

Another way of extending absorption to visible region is through dye sensitization, such as polymers [16–19] and metal–organic complexes [20,21] modified TiO_2 . As these dyes sensitized TiO_2 produce hydroxyl radicals (•OH) through trapping conduction band electrons to reduce oxygen to superoxide, many dyes cannot withstand this severe oxidative stress for long time. So from the point of remedying the environment, it is desired to develop new sensitization system with high activity, visible-response, and high stability.

In order to avoid dye decomposition in the degradation progress of pollutants, the dye should be not mixed with pollutants. At the same time, electron induced by light through dye could be separated from positive charge and transferred to pollutants solution. Based on this idea, a thin film of TiO₂ with bifunctionalized zones was designed. One zone was sensitized by a dye, namely dye-sensitized zone. The other was used for insertion into pollutants solution for degradation, namely degradation zone. In the dye-sensitized zone, a similar structure of dye-sensitized solar cells (DSSCs)[22,23] was fabricated to segregate the dye from pollutants. Here we hope to report the result of degradation of 4-chlorophenol (4-CP) with the bifunctionalized TiO₂ film under visible light irradiation.

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Fig. 1. The procedure for preparation of bifunctionalized TiO₂ film. (A) Glass sheet ($16 \text{ mm} \times 36 \text{ mm}$, FTO or OR); (B) 1 μ m thick TiO₂ film by screen printing; (C) a area of TiO₂ film ($14 \text{ mm} \times 14 \text{ mm}$) with 5 μ m thickness; (D) TiO₂ film sensitized by N719 dye; (E) the dye-sensitized TiO₂ surrounded by surlyn sealing film; (F) covering Pt-I and injecting electrolyte.

2. Experimental details

2.1. Preparation of bifunctionalized TiO₂ film

The bifunctionalized TiO₂ film was composite of a dyesensitized zone and a degradation zone, which was prepared as shown in Fig. 1. TiO₂ colloid was prepared according to the literature method [24], which was used for the preparation of the nanocrystalline films. The TiO₂ paste consisting of 18 wt% TiO₂, 9 wt% ethyl cellulose and 73 wt% terpineol was firstly prepared, which was printed on a glass sheet using a screen printing technique. FTO conducting glass sheet ($16 \text{ mm} \times 36 \text{ mm}$, fluorine doped SnO₂, sheet resistance 10 Ω /sq, transmission > 90% in the visible) or an ordinary glass sheet (OR) was cleaned by a standard procedure [24]. The thickness of the TiO₂ film was controlled by repetition of printing. The film was dried in air at 120 °C for 30 min and calcined at 500 °C for 30 min under flowing oxygen before cooling to room temperature. A area of TiO₂ film $(14 \text{ mm} \times 14 \text{ mm})$ with ca. 5 μ m thickness was stained by immersing it into a dye solution containing 300 μ M cis-Ru(dcbpy)₂(NCS)₂ (N719) as dye sensitizer, which is among the best photosensitizers used in mesoporous TiO₂-based dye sensitized solar cells (DSSCs). After 48 h at room temperature, the dye-stained film was rinsed with dry ethanol and dried by a dry air flow. Pt was deposited on FTO glass by coating with a drop of H₂PtCl₆ solution (40 mM in ethanol) with heat treatment at 395 °C for 15 min to give a Pt electrode, coded as Pt-I. The dyesensitized TiO₂ film and Pt-I electrode were separated by a surlyn spacer film (50 μ m thick) and sealed by heating to form a sandwich type cell. Electrolyte was then injected into the cell gap to form bifunctionalized TiO₂ film. The electrolyte was a solution of 0.6 M 1,2-dimethyl-3-n-propylimidazolium iodide (DMPImI), 0.1 M LiI, 0.05 M I₂, and 0.5 M tertbutylpyridine in acetonitrile.

2.2. The degradation experiment of 4-chlorophenol

The degradation experiment was conducted in a wide-mouth glass flask reactor with 14 mL of 4-CP and magnetically stirred by a Teflon stirrer. The degradation zone of bifunctionalized TiO₂ film was immersed into the solution of 4-CP. Another Pt electrode, coded as Pt-II, was placed at a distance of 5 mm to the TiO₂ film and connected with the Pt-I electrode by a copper conductor wire, as shown in Fig. 2. A 300 W Xe lamp (L25, λ_{max} = 500 nm) was used as the visible light source, which was irradiated at a distance of 20 cm to the dye-sensitized zone of TiO₂ film through 420 nm cutoff filters. Air was bubbled through the pipe during the reaction. Light intensity, as measured by a visible-irradiance meter, was about 4.0 mW/cm² at the position of the TiO₂ film located. The concentration of 4-CP was determined by a HPLC using an Agilent 1100 chromatograph

equipped with a ZORBAX Eclipse XDB-C18 reversed phase column. HPLC was detected by a UV detector adjusted to 280 nm. The mobile phase was a mixture of water and methanol (20:80,v/v) with a flow rate of 1.0 mL/min. The total organic carbon (TOC) was measured using SHIMADZU TOC-VCPH instrument to evaluate the mineralization degree of 4-CP. The 2 M HCl and 2 M NaOH solutions were used to adjust pH to the desired values.

3. Results and discussion

3.1. Effect of substrates for the bifunctionalized TiO_2 film

In our initial degradation of 4-CP, two types of TiO₂ film were fabricated and investigated. One was TiO₂ deposited on an ordinary glass (OR). The other was TiO₂ on a FTO conducting glass. The typical degradation reaction was carried out under the conditions of 20 mg/L 4-CP, pH 4, bubbling air 5 L/h, and visible light intensity 4.0 mW/cm^2 . The variation of relative concentration of 4-CP (C_t/C_0) as a function of reaction time was shown in Fig. 3. It was obviously



Fig. 2. Photocatalytic degradation of 4-chlorophenol under visible light irradiation. (1) Visible light ($\lambda \ge 420$ nm); (2) dye-sensitized TiO₂ film; (3) ordinary glass sheet or FTO glass; (4) TiO₂ film without dye sensitization (degradation zone); (5) magnetic stirrer; (6) sealing film; (7) copper wire; (8) bubbling pipe; (9) Pt-II electrode; (10) Pt-I electrode; (11) electrolyte; (12) wide-mouth glass flask with 4-CP solution.



Fig. 3. Effect of two substrates for the bifunctionalized TiO_2 film on the degradation of 4-CP. \bullet : TiO_2 deposited on an ordinary glass (TiO_2/OR); \blacktriangle : TiO_2 on a FTO conducting glass (TiO_2/FTO); \blacksquare : TiO_2/OR , Pt-II electrode not connected with Pt-I electrode.

illustrated that the TiO₂ film on an ordinary glass exhibited significant activity for the removal of 4-CP. The concentration of 4-CP decreased 88% after 5 h under visible light irradiation. However, when 4-CP was degraded using the TiO₂ deposited on a FTO conductor glass, only 13% removal of the concentration of 4-CP was obtained under the same conditions. The reduction rate of total organic carbon (TOC) was slower than that of the degradation of 4-CP. The concentration of TOC decreased 38% after 5 h for the TiO₂ film on the ordinary glass sheet. The slow mineralization was due to the formation of aromatic intermediates in the process of degradation, which concentrations remain almost unchanged [25,26]. The results indicated that the TiO₂ deposited on the ordinary glass was efficient for the degradation of 4-CP under the reaction conditions. So the following experiments were performed by the TiO₂ film on an ordinary glass sheet.

3.2. Effect of Pt-II electrode

The effect of Pt-II electrode was studied on the basis of the bifunctionalized TiO₂ film. The degradation became a little slower under the typical degradation conditions when Pt-II electrode was not connected with Pt-I electrode in the absence of copper wire. The concentration of 4-CP decreased 80% after 5 h under visible light irradiation, and the variation concentration of 4-CP was shown in Fig. 3 as well. The relative low degradation efficiency implied that the Pt-II electrode had a positive effect on degradation performance when it was connected with Pt-I electrode by copper wire. To further show the degradation effect of Pt-II electrode, the bifunctionalized TiO₂ film and Pt-II electrode were inserted into two wide-mouth glass flask reactors A and B, respectively, as shown in Fig. 4. The two reactors with 14 mL of 4-CP and stirrer bar were carried out under the same conditions of 20 mg/L 4-CP, pH 4, bubbling air 5 L/h, and light intensity 4.0 mW/cm². The results were shown in Fig. 5. The reactor A degraded by the bifunctionalized TiO₂ film gave 81% removal of 4-CP after 5 h and almost no degradation of 4-CP (7% removal) was observed in the reactor B by the Pt-II electrode when degradation reaction was carried out in the absence of copper wire. The slight removal of 4-CP in the reactor B may be due to the absorption of Pt-II electrode surface. It was found that when Pt-II electrode was connected with Pt-I electrode by a copper wire, the concentration of 4-CP in the reactor B decreased 85% after 5 h and a little enhanced degradation efficiency was achieved in the reactor A (87% versus 81%). Degradation reaction occurring



Fig. 4. Degradation of 4-CP performed in separate reactors A and B.

in reactor B showed that Pt-II electrode produced active species, causing the decomposition of 4-CP. At the same time, degradation in reactor B promoted the degradation in reactor A.

3.3. Effect of ferrous ions

Ferrous ions have a remarkable promoting effect on degradation reaction in the Fenton process, which involves the reaction of Fe²⁺ with hydrogen peroxide (H₂O₂), giving rise to hydroxyl radicals. If hydrogen peroxide was generated in our degradation conditions, addition of FeSO₄ would promote the degradation of 4-CP. The effect of ferrous ions by addition of 0.5 mM FeSO₄ in reactors A and B was shown in Fig. 6. After irradiation of 5 h, the removal of 4-CP in reactors A and B was obtained in 97% and 96%, respectively, when adding 0.5 mM FeSO₄ in reactor A but no FeSO₄ in reactor B. The removal of 4-CP in both reactors was greatly accelerated by the presence of FeSO₄ in reactor A. However, their degradation efficiencies were not enhanced by the addition of FeSO₄ in reactor B. For example, 87% and 88% of 4-CP were removed in reactors A and B, respectively, when adding 0.5 mM FeSO₄ in reactor B and no FeSO₄ in reactor A. These results demonstrated that formation of hydroxyl radicals was promoted by the addition of Fe²⁺ in reac-



Fig. 5. Effect of Pt-II electrode on the removal efficiency of 4-CP in separate reactors A and B.



Fig. 6. Effects of Fe^{2+} and O_2 on the removal efficiency of 4-CP in separate reactors A and B. (a) Degraded by TiO_2 film in reactor A; (b) degraded by Pt-II electrode in reactor B.

tor A, resulting in enhanced degradation efficiency. The addition of $FeSO_4$ in reactor B had no obvious enhancement of the degradation efficiency, indicating that there was no H_2O_2 involved in this case.

3.4. Effects of O₂

To obtain insight into the role of O_2 in the present study, experiments under O_2 and N_2 atmospheres were undertaken. In the atmosphere of N_2 by bubbling nitrogen in reactors A and B, the degradation reaction in both reactors did not occur after 5 h under our reaction conditions. It was found that degradation reaction occurred and the removal of 4-CP in both reactors was obtained in 95% and 92%, respectively, when bubbling air in reactor A and bubbling nitrogen in reactor B (Fig. 6). However, when bubbling nitrogen in reactor A and bubbling air in reactor B, almost no degradation reaction was observed in the reactor A, nor did degradation in the reactor B. These results clearly demonstrated that the presence of O_2 was crucial for degradation in reactor A, but was not crucial for reactor B.

3.5. Degradation mechanism

A schematic mechanism for the degradation reaction was shown in Fig. 7. In dye-sensitized zone, light absorption takes place in the dye under irradiation, with subsequent electron transfer from the dye's excited states (dye^{*}) into the conduction band (CB) of



Fig. 7. Working principle of the degradation system.

the TiO_2 . As for the TiO_2 film deposited on an ordinary glass, the electrons transport to the degradation zone via diffusion of electrons through the network of TiO₂ nanoparticles. The oxidized dyes (dye⁺) are regenerated by the iodidie/triiodide redox couple through reactions of Eqs. (1) and (2), followed by electron exchange transporting the positive charge to the Pt-I electrode via Eq. (3). In degradation zone, the electron transporting at conduction band of TiO₂ is at high energy level and can react with oxygen in solution to produce $O_2^{\bullet-}$, followed by reaction with H⁺ to form high active species of hydroxyl radicals (•OH) through Eqs. (4)-(8) for degradation of 4-CP [27]. As for the TiO₂ film deposited on a FTO conducting glass, electrons generated in dye-sensitized zone prefer transporting through FTO conducting glass rather than through semiconductor TiO₂ film because the former has superior conductivity to the latter. Thus, electrons transfer through FTO conducting glass from the dye-sensitized zone to the degradation zone. It is known that the resistance of TiO₂ is much higher than that of FTO glass. Therefore, the electrons in degradation zone are hard to arrive at the surface of TiO₂ film because there is no sufficient driving force for electron injection from FTO glass to TiO₂ surface under the reaction conditions. Few electrons at the surface of TiO₂ film afford few active species, which results in low degradation efficiency. Therefore, the reason for high degradation efficiency of TiO₂ film based on the ordinary glass is that electrons induced by light directly transform from the dye-sensitized zone to the degradation zone through the TiO₂ film.

$$3I^- \rightarrow I_3^- + 2e^- \tag{1}$$

$$2dye^+ + 2e^- \rightarrow 2dye \tag{2}$$

 $I_3^- + 2e^- \rightarrow 3I^-$ (3)

 $O_2 + e_{CB} \rightarrow O_2^{\bullet-} \tag{4}$

 $O_2^{\bullet-} + H^+ \to HOO^{\bullet}$ $HOO^{\bullet} + e_{CD}^{-} \to HOO^{-}$ (5)

$$100 + C_B \rightarrow 100 \tag{0}$$

 $HOO^{-} + H^{+} \rightarrow H_{2}O_{2} \tag{7}$

$$H_2O_2 + e_{CB}^- \rightarrow HO^- + HO^{\bullet}$$
(8)

Pt-II electrode had an important affection on the degradation. In the reported electrochemical degradation method, hydroxyl radicals (•OH) generally was produced at the surface of a highly oxidized overvoltage anode from water oxidation via Eqs. (9) and (10) [28,29]. The active species of either physically adsorbed hydroxyl radical (•OH) or chemisorbed metal oxide (MO) in the lattice of metal may be formed from water discharge along with electron release [8]. The degradation by Pt-II electrode working smoothly in reactor B showed that there was highly oxidized overvoltage on the electrode. The high overvoltage on the Pt-II electrode should be originated from the oxidized dyes with the positive charge transfer through the iodide/triiodide redox couple to the Pt-I electrode. The oxidized dye was regenerated by reduction reaction with I-, and Iwas converted to I_3^- (Eqs. (1) and (2)). When I_3^- was catalytically converted into I⁻ through Pt-I electrode with electron exchange, positive charge was transported from Pt-I to Pt-II through copper wire. As dyes repeated the process of light absorption and regeneration, the oxidized overvoltage of the Pt-II electrode with arrival of the positive charges from the Pt-I electrode became high enough for production of •OH through water oxidation. Then the degradation reaction by the Pt-II electrode occurred. Moreover, in the process of Pt-II electrode production of •OH, electron was released from water oxidation and reacted with I₃⁻ to generate I⁻ via Pt-I. If there is no electron supplied for the recover of I^- from I_3^- , the concentration of I⁻ in electrolyte would decrease and gradually be consumed. When the oxidized dyes were not regenerated in the absence of I⁻, the degradation reaction would stop. Therefore, the degradation by Pt-II electrode was driven by photo-generated positive charge in dye-sensitized TiO₂ film, and also afforded electron for regeneration of the oxidized dye, promoting the degradation of TiO₂ film.

$$Pt + H_2O \rightarrow Pt(\bullet OH) + H^+ + e^-$$
(9)

$$Pt(\bullet OH) \rightarrow Pt(O) + H^+ + e^-$$
(10)

FeSO₄ has an obvious influence on degradation reaction. Addition of Fe²⁺ in reactor A enhanced the degradation efficiency in reactors A and B. The bifunctionalized TiO₂ film in reactor A produced H₂O₂, which was promoted by Fe²⁺ to form active species HO• as shown in Eq. (11). More active species were generated, much higher degradation efficiency was achieved. The catalyst of Fe²⁺ could be regenerated through electrolysis reduction of Fe³⁺ via Eq. (12). The higher degradation efficiency in reactor A would consume more electrons, which would produce more positive charges for Pt-II and caused higher degradation efficiency in reactor B. Addition of Fe²⁺ in reactor B gave no enhancement in both reactors due to no formation of H₂O₂ in reactor B.

$$H_2O_2 + Fe^{2+} \to HO^{\bullet} + Fe^{3+}$$
 (11)

$$\mathrm{Fe}^{3+} + \mathrm{e}^{-} \to \mathrm{Fe}^{2+} \tag{12}$$

Oxygen is crucial for the degradation. The photogenerated electrons can reduce the adsorbed molecular oxygen on the TiO₂ surface to produce $O_2^{\bullet-}$, followed by reaction with H⁺ to form superoxide radical anion HOO[•]. The high active species of hydroxyl radicals (•OH) are generated through Eqs. (5)–(8) [27,30]. It is known that •OH radicals are nonselective and strong electrophilic oxidizing species [31]. When bubbling N₂ in reactor A, no active species was formed in the absence of O₂, leading to no degradation. On the other hand, electrons at conduction band of TiO₂ could not be consumed without O₂ and would come back to the dye cation with recombination or into electrolyte solution reacting with I₃⁻ [32]. The positive charge transported into Pt-I electrode would be limited and the oxidized overvoltage on the Pt-II electrode would not be accumulated enough high to oxidize H₂O to form hydroxyl radicals. Therefore, when bubbling nitrogen in reactor A,

the degradation reaction did not occur in reactor A, neither did in reactor B.

For the practical application of such bifunctionalized TiO_2 film, not only the degradation efficiency is important, but its durability or lifetime is also critical. The degradation of 4-CP for five recycles of the bifunctionalized TiO_2 film was tested. The degradation effectiveness decreased from 98% to 92% after five repeated uses, which demonstrated the as-prepared bifunctionalized TiO_2 film was comparably stable under the studied conditions.

4. Conclusions

A new bifunctionalized TiO₂ film was designed for degradation of 4-CP under visible light irradiation. The bifunctionalized TiO₂ film was composite of an area of dye-sensitized TiO₂ film and an area of un-sensitized TiO₂ film. The effects of substrates for TiO₂ film, Pt-II electrode, FeSO₄, and O₂ on degradation of 4-CP were studied. When the bifunctionalized TiO₂ film was deposited on an ordinary glass sheet, the concentration and TOC of 4-CP decreased 88% and 38%, respectively, after 5 h irradiation at initial concentration of 20 mg/L, pH at 4, and light intensity of 4.0 mW/cm^2 with bubbling air. The concentration of 4-CP decreased only 13% when TiO₂ film was deposited on a FTO conducting glass under the same conditions. Pt-II electrode afforded comparable degradation efficiency when it was connected with Pt-I electrode by a copper. The degradation efficiency could be improved by addition of FeSO₄ which promoted H₂O₂ to form •OH. Oxygen is crucial for the degradation reaction. The as-prepared device was comparably stable in the process of degradation after five recycles. The device worked smoothly for degradation of 4-CP under visible light irradiation without external power supply. This process is promising for degradation of organic pollutants due to its saving-energy, low cost, and sustainability.

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